

Impact of Nanoparticle Characteristics on Heat Transfer Enhancement for Industrial Cooling Applications: A Comparative Study of Thermal Conductivity Models

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Abstract:

In the extrusion of polymer sheets cooling the surfaces quickly and uniformly is one the most critical activity. Conventional methods of cooling using chill rolls can be improved by embedding nanofluids. This current article is aimed at analysing the heat transport in carbon nanotubes-based nanofluid by two advanced thermal conductivity models namely, the Yamada–Ota and Xue models. Among the most significant physical properties in the polymer extrusion and stretching sheet cooling process is the thermal conductivity, which defines the rate at which heat can be removed from the hot polymer sheet during cooling. This is crucial for controlling the solidification, thickness, and mechanical properties of the final film. The mathematical model is framed according to boundary layer approximation theory for momentum and energy equations and solved by MATLAB solver bvp4c. The study investigates the effects nanoparticle volume fraction, magnetic field strength, wall thickness variation, power-law index, and thermal relaxation time on momentum and energy profiles, with results presented graphically. The novel outcomes of this study shows that the Yamada–Ota model demonstrates 30.60% higher heat transfer rate compared to the Xue model for nanoparticle volume fraction $\phi = 0.03$ and $m = 1.5$.

Key words: Hybrid nanofluid, variable thickness surface, MATLAB, numerical analysis.

1. Introduction.

Recent advances in the field on Nanotechnology fascinated many researchers to investigate more advanced nanofluids. The proficiency of the nanofluids in the enhancement of Heat transfer and Thermal conductivity by adding Nanoparticles like copper, alumina, gold, silver to the base fluids such as ethylene glycol, water have many applications in Biomedicine, nuclear reactors, food Industries, chemical Industry, automobiles, electronics etc. Xuan and Li [1] studied enhancement of heat transfer of nanofluids in tube by suspending solid nanoparticles. A comparative study of mass and heat transfer in non-Newtonian fluids over a permeable stretching sheet is coated by Sandeep et al. [2]. Raju et al. [3] theoretically investigated mass and heat transfer of nanofluids over a cone considering the parameters magnetic effect, non-uniform heat source/sink and concluded that heat transfer rate is more in Maxwell and oldroyd -B nanofluids compared to Jeffrey nanofluid. Qureshi [4] studied radiative heat and mass transfer MHD nanofluid flow in the presence spherical Au-metallic nanoparticles. Sugunamma et al. [5] reported 3-D motion of heat transfer in two different ferro liquids.

Reddy et al. [5] explored their study on Casson fluid suspended with Fe_3O_4 nanoparticles over an upper surface of paraboloid of revolution. Stagnation point flow of $\text{SiO}_2\text{-Al}_2\text{O}_3$ hybrid nanofluid for mixed convection parameter is investigated and dual solutions is obtained by [6]. Various applications of nanoparticles is explored by Khan et al. [7], and Boundary layer flow of nanofluid with magnetic effect.

Magnetohydrodynamic (MHD) effect has received a lot of attention by many authors in recent years due to its wide applications in the cooling process of a nuclear reactor, power generator, control of chemical waste and pollutants dissemination, and metallurgical applications. The entropy analysis of Boundary layer nanofluid flow with MHD effect over porous shrinking sheet is investigated by Rashid et al. [8]. The effect of hybrid nanofluid flow with MHD and Radiation past a shrinking sheet were proposed by Waini et al [9]. Ramana reddy et al [10] studied the impact of 3D MHD flow of ferrofluids, methanol & kerosene over a stretching a sheet considering nonlinear radiation and concluded that sundry physical quantities viscosity and nonlinear radiation parameters affects the flow. A similar

study carried out by Punit Gowda et al [11]. They explored that a 2D ferromagnetic fluid flow over a stretching sheet with the magnetic dipole effect. Marangoni convection is characterized as interface dissipative flow. Marangoni convection is produced due to variation in surface tension gradients, Recently Magneto-Marangoni convection boundary layer flow has attracted many researchers for its numerous applications in material science, chemical engineering, food industry, welding, thin liquid films etc. Marangoni convection phenomenon is widely used in art work. Vishnu Ganesha et al [12] numerically investigated the behavior Marangoni boundary layer flow of $\gamma\text{-Al}_2\text{O}_3$ nanoparticles suspended in ethylene glycol and water base fluids in the presence of magnetic field and nonlinear thermal radiation. P. Dadheech et al. [13] investigated the effect of Marangoni convection of gamma-alumina oxide nanofluid past porous stretching sheet in the presence of thermal radiation and magnetic field. Y. Lin et al [14] investigated Marangoni boundary layer flow of Cu-H₂O nanofluid with exponential temperature and radiation effect over geometric shapes and concluded that sphere shaped nanoparticle with lesser thermal conductivity has better heat transfer enhancement compared to other shaped nanoparticles. Hayat et al. [15] addressed the impact of carbon-water nanoparticles with thermal radiation effect on Marangoni convection with boundary layer flow. A similar study of Marangoni convection is carried out by many researchers considering different circumstances see refs [16]–[26]. The flow past a porous medium has significant applications in the field of material processing, geothermal energy, drying processes, fuel cell machineries, oil recovery, medical sciences, earth sciences and various industries. S. Mukhopadhyay et al.[27] studied the effects of thermal radiation and variable viscosity of convective boundary layer flow past porous stretching sheet. K.Khanafar and K.Vafai [28] presented their review on nanofluids applications in porous medium. Dadeech et al. [29] investigated the Marangoni convective heat transfer effect of hybrid nanofluid flow of Copper Oxide-Silver nanoparticles with base fluid ethanol glycol passed through a porous stretching sheet.

Prandtl number is a dimensionless number, the ratio of momentum diffusivity to thermal diffusivity. Vishnu Ganesh et al [30] presented a numerical study of thermal transport characteristics of $\gamma\text{-Al}_2\text{O}_3$

nanofluids over a Riga plate and analyzed the boundary layer flow and viscosity using an effective Pr number model. A similar study over a channel is conducted by Saba et al [31]. A similar effective Pr number models for $\gamma\text{-Al}_2\text{O}_3 / \text{H}_2\text{O}$. and $\gamma\text{-Al}_2\text{O}_3 / \text{C}_2\text{H}_6\text{O}_2$ nanofluids is analysed by Rashidi et al [32], Gul et al [33] experimentally studied the the phenomena of spray distribution on stretching cylinder using $\gamma\text{-Al}_2\text{O}_3$, Cu- H₂O based nanofluids. The optimal scheme model resulted the impact of effective Pr number. A Zaib et al [34] explored the influence of effective Pr number on mixed convective micropolar flow of gamma alumina oxide-water nanofluid driven from wedge. Numerical investigation of effective Pr number of gamma alumina oxide nanoparticles with magneto hydrodynamic effect of boundary layer flow over the melting stretching sheet was put forth by N Ganesh et al [35]. Qayyum & Sumaira [36] illustrated the effects of MHD & Marangoni convection over a hybrid nanofluid suspending copper nanoparticles in water and ethylene glycol base fluids. To the best of author knowledge, no investigation is reported on variable thickness stretching sheet with Yamada-Ota and Xue model utilising nanofluid using non-Fourier heat flux model.

2. Mathematical formulation.

Let us consider boundary layer flow in two-dimensional coordinate configuration in which variable thickness sheet is considered in x axis direction and y axis is taken perpendicular to flow direction. Detailed configuration is shown in figure 1. The following assumptions are used in this mathematical modelling.

Slendering surface moving velocity is considered as $u_w(x) = A_0(x + b)^m$ where A_0 and b are constants. The thickness of stretching sheet decreases in x axis direction and it is written in the form $y(x) = A_1(x + b)^{\frac{1-m}{2}}$ where A_1 stretching constant. Under the above-mentioned assumption, the boundary layer equations can be expressed in Cartesian coordinate system as:

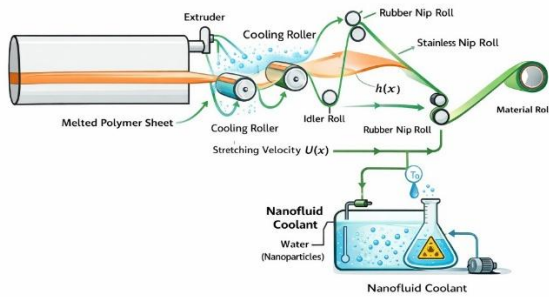


Figure 1: Extrusion model and fluid flow configuration

$$\frac{\partial \tilde{u}}{\partial x} = -\frac{\partial \tilde{v}}{\partial y} \quad (1)$$

$$\tilde{u} \frac{\partial \tilde{u}}{\partial x} + \tilde{v} \frac{\partial \tilde{u}}{\partial y} = \frac{\mu_{nf}}{\rho_{nf}} \frac{\partial^2 \tilde{u}}{\partial y^2} - \frac{\sigma_{nf}}{\rho_{nf}} B_0^2 \tilde{u} \quad (2)$$

$$\begin{aligned} \tilde{u} \frac{\partial \tilde{T}}{\partial x} + \tilde{v} \frac{\partial \tilde{T}}{\partial y} &= \frac{k_{nf}}{(\rho c_p)_{nf}} \frac{\partial^2 \tilde{T}}{\partial y^2} - \lambda_T \left(\tilde{u}^2 \frac{\partial^2 \tilde{T}}{\partial x^2} + \tilde{v}^2 \frac{\partial^2 \tilde{T}}{\partial x^2} + \right. \\ &\quad \left. 2\tilde{u}\tilde{v} \frac{\partial^2 \tilde{T}}{\partial x \partial y} + \tilde{u} \frac{\partial \tilde{u}}{\partial x} \frac{\partial \tilde{T}}{\partial x} + \tilde{u} \frac{\partial \tilde{v}}{\partial x} \frac{\partial \tilde{T}}{\partial y} + \tilde{v} \frac{\partial \tilde{u}}{\partial y} \frac{\partial \tilde{T}}{\partial x} + \tilde{v} \frac{\partial \tilde{v}}{\partial y} \frac{\partial \tilde{T}}{\partial y} \right) \end{aligned} \quad (3)$$

2.1. Boundary conditions.

$$\tilde{u} = u_w(x) = A_0(x+b)^m, \tilde{T} = T_w(x), \tilde{v} = 0 \quad \text{at} \quad y = A_1(x+b)^{\frac{1-m}{2}}$$

$$\tilde{u} \rightarrow 0, \tilde{T} \rightarrow T_\infty \quad \text{as} \quad y \rightarrow \infty \quad (4)$$

with velocity components in the x and y directions as $\tilde{u}$ and $\tilde{v}$ respectively. λ_T is the thermal relaxation time, μ_{nf} denotes dynamic viscosity, k_{nf} is thermal conductivity of nanofluid, ρ_{nf} is density of nanofluid and $(c_p)_{nf}$ denotes nanofluid heat capacity. Let us introduce a similarity variable ξ to reduce multivariable differential equations in terms of single variable ξ

$$\tilde{u} = A_0(x+b)^m F'(\xi), \quad \tilde{v} = -\sqrt{\frac{(m+1)}{2}} v_f A_0(x+b)^{\frac{m-1}{2}} \left(F(\xi) + \xi F'(\xi) \frac{m-1}{m+1} \right)$$

$$\begin{aligned} \psi(\xi) &= F(\xi) \sqrt{\frac{2}{m+1}} v_f A_0(x+b)^{\frac{m+1}{2}}, \quad \theta(\xi) = \\ &= \frac{\tilde{T} - \tilde{T}_\infty}{\tilde{T}_w - \tilde{T}_\infty}, \quad \xi = y \sqrt{\frac{(m+1)}{2 v_f}} A_0(x+b)^{\frac{m-1}{2}} \end{aligned} \quad (5)$$

Hence by stream function, the velocity terms can be expressed as $\tilde{u} = \frac{\partial \psi}{\partial y}$ and $\tilde{v} = -\frac{\partial \psi}{\partial x}$. Using the similarity transformations (5) in equations (2)

$$, (3) \text{ and } (4), \quad F''' + \frac{A_2}{A_1} \left(FF'' - \frac{2m}{m+1} F'^2 \right) - \frac{A_5}{A_1} M \left(\frac{2}{m+1} \right) F' = 0 \quad (6)$$

$$\begin{aligned} \theta'' + \text{Pr} \frac{A_3}{A_4} F\theta' + \gamma \text{Pr} \frac{A_3}{A_4} \left(\frac{m-3}{2} FF'\theta' - \right. \\ \left. \frac{m+1}{2} F^2\theta'' \right) = 0 \end{aligned} \quad (7)$$

and boundary conditions can be written as

$$\begin{aligned} F(\alpha) &= \alpha \left(\frac{1-m}{1+m} \right), F'(\alpha) = 1, \theta(\alpha) = 1, F'(\infty) = \\ 0, \theta(\infty) &= 0 \end{aligned} \quad (8)$$

The parameter $\alpha = A_1 \sqrt{\frac{m+1}{2 v_f}} A_0$ is defined as the wall thickness.

Setting $\eta = \xi - \alpha$, $F(\xi) = F(\xi - \alpha) = f(\eta)$ and $\theta(\xi) = \theta(\xi - \alpha) = \theta(\eta)$. The equations (6)-(8) becomes

$$f''' + \frac{A_2}{A_1} \left(ff'' - \frac{2m}{m+1} f'^2 \right) - \frac{A_5}{A_1} M \left(\frac{2}{m+1} \right) f' = 0 \quad (9)$$

$$\begin{aligned} \theta'' + \text{Pr} \frac{A_3}{A_4} f\theta' + \gamma \text{Pr} \frac{A_3}{A_4} \left(\frac{m-3}{2} ff'\theta' - \frac{m+1}{2} f^2\theta'' \right) = \\ 0 \end{aligned} \quad (10)$$

With the following boundary conditions,

$$f(\eta) = \alpha \left(\frac{1-m}{1+m} \right), \frac{\partial f}{\partial \eta} = 1, \theta(\eta) = 1 \quad \text{at} \quad \eta = 0$$

$$\frac{\partial \theta}{\partial \eta} = 0, \theta = 0 \quad \text{at} \quad \eta = \infty \quad (11)$$

here m is power index of velocity, M is magnetic parameter, wall thickness parameter α , Prandtl number Pr and Thermal relaxation time γ , are the non-dimensional parameters that appear in equations (12)-(14). These parameters are defined as

$$M = \frac{\sigma_f B_0^2 (x+b)}{\rho_f u_w}, \alpha = A_1 \sqrt{\frac{m+1}{2 v_f}} A_0, \text{Pr} = \frac{v_f (\rho c_p)_f}{k_f}, \gamma = \lambda_T A_0 (x+b)^{m-1}$$

The expression for A_1, A_2, A_3, A_4 & A_5 appearing in equations (9)-(11) due to the nanofluid is given

$$\begin{aligned} \text{as } A_1 &= \frac{\mu_{nf}}{\mu_f}, A_2 = \frac{\rho_{nf}}{\rho_f}, A_3 = \frac{(\rho c_p)_{nf}}{(\rho c_p)_f}, A_4 = \frac{k_{nf}}{k_f}, \\ A_5 &= \frac{\sigma_{nf}}{\sigma_f}, \end{aligned}$$

Xue thermal conductivity model⁵²

$$\frac{k_{nf}}{k_f} = \frac{1 - \phi - 2\phi \left(\frac{k_{np}}{k_f - k_{np}} \right) \ln \left(\frac{k_f + k_{np}}{2k_f} \right)}{1 - \phi - 2\phi \left(\frac{k_f}{k_f - k_{np}} \right) \ln \left(\frac{k_f + k_{np}}{2k_f} \right)}$$

Yamada-Ota thermal conductivity model ⁵²

$$\frac{k_{nf}}{k_f} = \frac{\frac{k_{np}}{k_f} + 2\phi^{0.2} \frac{L}{R} - 2\phi\phi^{0.2} \frac{L}{R} \left(1 - \frac{k_{np}}{k_f} \right)}{\frac{k_{np}}{k_f} + 2\phi^{0.2} \frac{L}{R} + \phi \left(1 - \frac{k_{np}}{k_f} \right)}$$

Here, K denotes the shape factor, which for cylindrical particles is given by the expression $K = 2\phi^{0.2} \frac{L}{D}$. where L and D represent the length and diameter of the cylindrical particles, respectively. According to the measurements reported in [53], the average length and diameter of the carbon nanotubes (CNTs) are approximately $10 \mu\text{m}$ and 150 nm . The subscripts f , nf and np denote base fluid, nanofluid and nanoparticle respectively. Thermo-physical properties of water and nanoparticle is listed in Table 1.

Table 1: Thermo-physical properties of water and nanoparticle ⁵³

Thermo-physical properties	$\rho(\text{kg}/\text{m}^3)$	$C_p(\text{J}/\text{kg K})$	$k(\text{W}/\text{m K})$	$\sigma(\text{S}/\text{m})$
Water	997.1	4179	0.613	0.05
CNT	2600	425	6600	0.5×10^{-6}

The skin friction coefficient(C_{fx}) at the surface and the Nusselt number (Nu_x) are $C_{fx} = \frac{\tau_w}{\rho_f u_w^2}$, $Nu_x = \frac{(x+b)\theta_w}{k_f(T_w - T_\infty)}$ after simplification of shear stress and heat flux terms and using similarity variable the non-dimensional form of these two physical quantities can be written as:

$$\sqrt{Re_x} C_{fx} = A_1 \sqrt{\frac{m+1}{2}} f''(0) \quad (14)$$

$$Nu_x Re_x^{-1/2} = -A_4 \sqrt{\frac{m+1}{2}} \theta'(0) \quad (15)$$

where $Re_x = \frac{(x+b)U_w}{\nu}$ is local Reynold's Number.

3. Results and discussion.

In this research article, the authors investigated the effects ⁽¹²⁾ of various parameters, including the magnetic parameter, on the system under consideration. (M), volume fraction of nanoparticle (ϕ), wall thickness parameter (α) and thermal relaxation parameter(γ) on dimensionless profiles $f'(\eta)$, $\theta(\eta)$ and $Nu_x Re_x^{-1/2}$ is scrutinized through graphical representations. Except in plotting of graph, the values of influencing parameters are fixed as $M = 1, \phi = 0.02, \alpha = 0.1, \gamma = 0.1, Pr = 6.8$. The influence of the magnetic parameter (M) upon velocity is depicted in figures 2a & 2b. The magnetic parameter (M) represents the effect of a magnetic field on an electrically conducting fluid. From Figures 2a and 2b .It is noticed that magnetic parameter accelerates the momentum profile and also energy profile is diminished for higher values of magnetic parameter. Increasing the magnetic parameter (M) reduces the velocity and causes the fluid to diverge as it moves along the surface. The influence of the magnetic parameter in reducing velocity is more pronounced due to the spreading of the flow. When a magnetic field is applied, it induces a resistive force called the Lorentz force. This force opposes the motion of the fluid, thereby reducing the velocity even further. The influence of magnetic parameter on the temperature distribution under varying magnetic field strengths is depicted in Figures 3a and 3b. Increase in the magnetic parameter results in a reduction in velocity near the surface. This decrease thickens the thermal boundary layer and raises the surface temperature due to diminished convective heat transfer.

Figures 4a and 4b depict how varying the nanoparticle volume fraction affects the velocity distribution. As the volume fraction increases, the fluid velocity decreases, primarily due to heightened viscosity and increased resistance to flow. This contrasting behaviour is more prominently captured by the Yamada–Ota model, which more effectively accounts for nanoparticle interaction effects compared to the Xue model.

Figures 5a and 5b show the effects of nanoparticle volume fraction on the thermal profile. Increased nanoparticle concentration enhances thermal conductivity, leading to elevated temperatures near the surface and a thickened thermal boundary layer. However, convex sheets exhibit more substantial

temperature rises due to higher flow separation and drag. Concave sheets, maintaining better flow attachment, experience a comparatively moderate increase in temperature. Again, the Yamada–Ota model demonstrates a more significant sensitivity to these changes than the Xue model.

Figures 6a and 6b present the impact of the wall thickness parameter α on the velocity profile. For $m < 1$, increasing α decreases the stretching velocity, thereby reducing the flow velocity. For $m > 1$, while the stretching velocity increases with α , the added thickness may still introduce resistance near the surface, moderating the overall flow velocity. In both cases, a thicker wall tends to reduce the boundary layer thickness, thus altering the velocity distribution

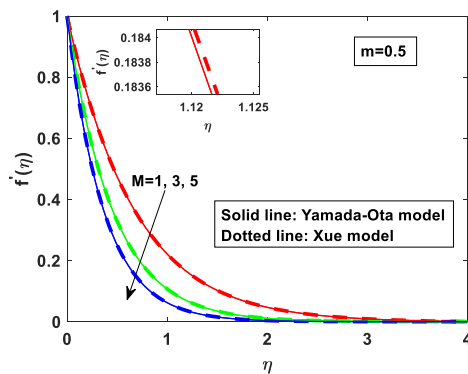


Figure 2a: Impact magnetic parameter on velocity for $m = 0.5$.

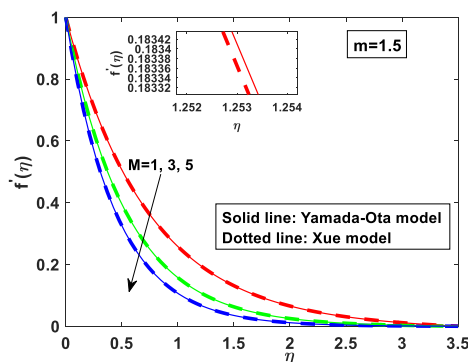


Figure 2b: Impact magnetic parameter on velocity for $m = 1.5$.

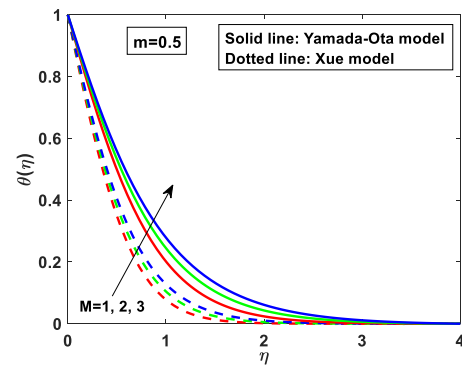


Figure 3a: Impact energy profile for $m = 0.5$.

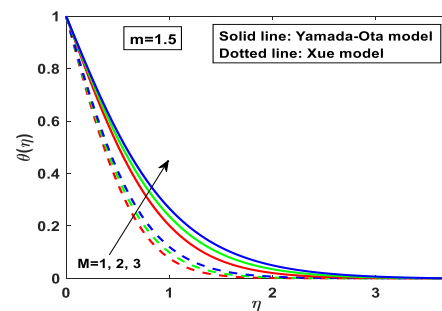


Figure 3b: Impact energy profile for $m = 0.5$.

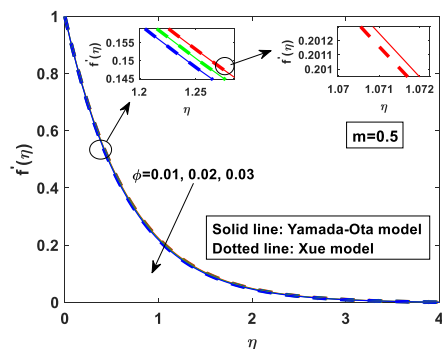


Figure 4a: Impact of nanoparticle volume fraction on velocity for $m = 0.5$.

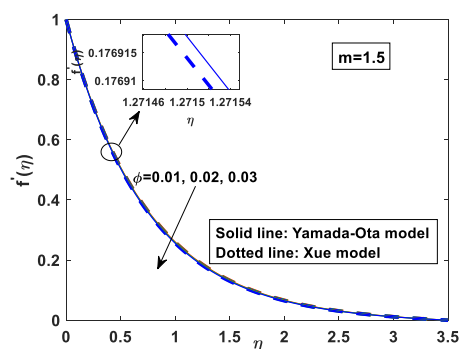


Figure 4b: Impact of nanoparticle volume fraction on velocity for $m = 1.5$.

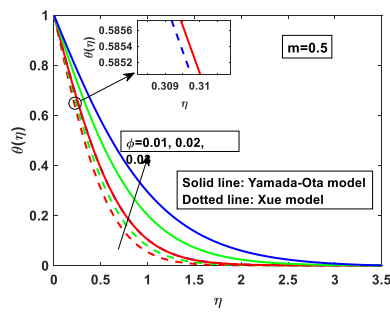


Figure 5a: Impact of nanoparticle volume fraction on temperature for $m = 0.5$.

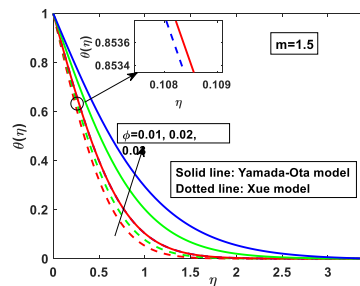


Figure 5b: Impact of nanoparticle volume fraction on temperature for $m = 1.5$.

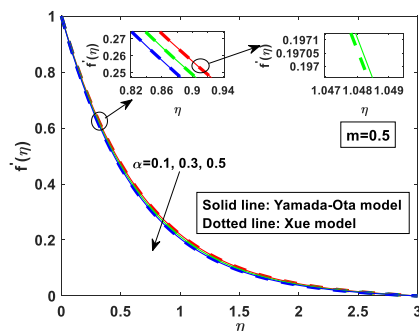


Figure 6a: Impact of wall thickness parameter on velocity for $m = 0.5$.

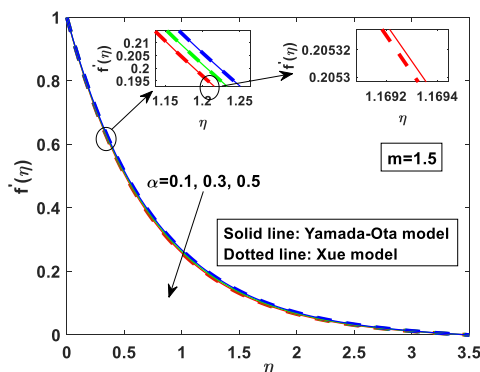


Figure 6b: Impact of wall thickness parameter on velocity for $m = 1.5$.

4. Concluding remarks.

The study investigates the influence of several parameters—magnetic field strength (M), nanoparticle volume fraction (ϕ), wall thickness (α), and thermal relaxation parameter (γ)—on the velocity and temperature profiles, as well as the Nusselt number in nanofluid systems. The effects are analysed for different sheet geometries, including convex ($m < 1$), concave ($m > 1$) sheets, using both the Xue and Yamada-Ota models.

- The temperature increases near the sheet with increasing M due to a thicker thermal boundary layer caused by reduced velocity.
- A higher value of wall thickness parameter α results in decreased velocity due to increased drag and flow separation.
- Temperature increases with thicker walls due to reduced convective heat transfer, with convex sheets showing a more pronounced rise in surface temperature.
- The Yamada-Ota model provides higher and more accurate predictions for heat transfer than the Xue model, particularly due to its better representation of CNT nanofluid properties.

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